



TO WHOM IT MAY CONCERN JANUARY 2024



PL Engineering and Technology Ltd

We know how and we just do it!





ENVIROMENTAL BENEFITS OF PLASMA GASIFICATION TECHNOLOGY

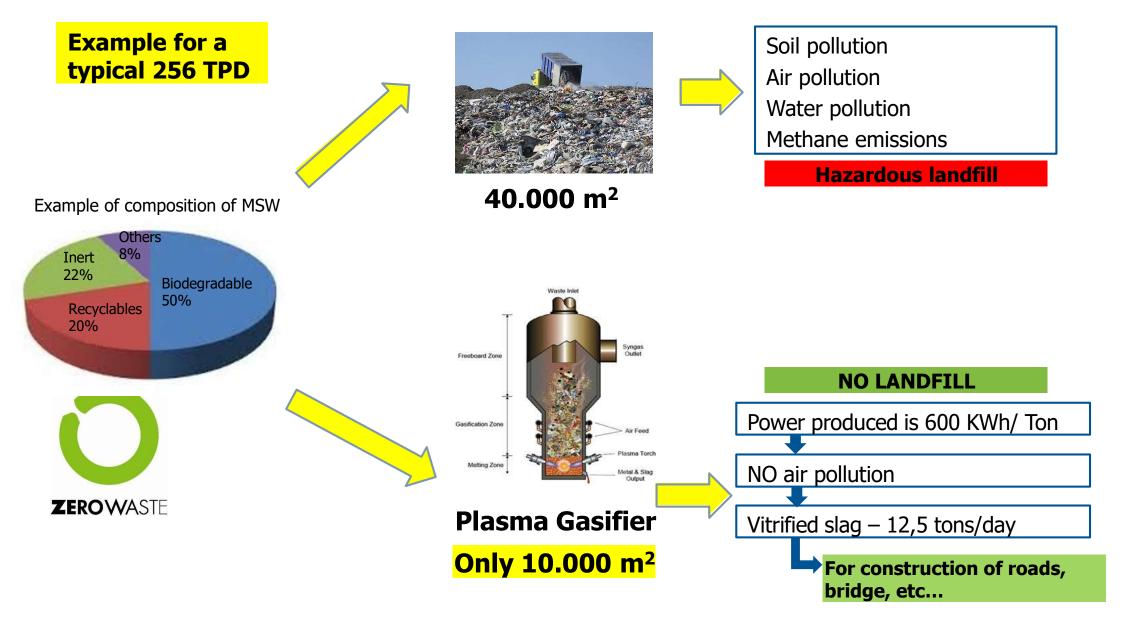
- The PL ET Ltd technology creates a syngas:
 - Which can be converted into power, steam, liquid fuels, hydrogen or fertilizer compounds
 - With very low quantities of NOx, Dioxins and Furans
- Non-gaseous, inorganic components are converted to molten slag which is removed as vitrified by-product, safe for use as a construction aggregate
- Potential to recycle fly ash back into gasifier for vitrification and reuse.
- Plasma gasification results in substantial net decreases in greenhouse gas (CO₂ equivalent) emissions versus traditional landfilling and incineration
- In a combined cycle process, sulfur and other contaminants in the syngas are removed by proven gas cleanup equipment before the syngas is converted into other energy products

NO LANDFILL VERY LOW EMISSIONS DURING THE PROCESS





ZERO WASTE SCENARIO





DIOXIN AND FURANS

Our plasma gasification process mitigates the formation of dioxins and furans :

- Dioxins & Furans form between 400-800°C, in our system the temperature of the syngas when it exits the gasifier is ~1,000-1,200°C, it is immediately quenched to temperatures below 400°C
- The Syngas does not remain in the temperature range where Dioxins and Furans form
- High residence times within the reactor ensure tars are cracked and minimize particulates from exiting with syngas stream



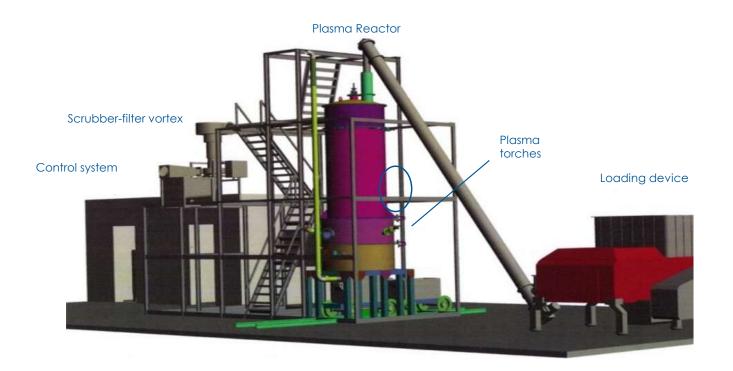
MIHAMA-MIKATA VITRIFIED SLAG

 Slag from the Mihama-Mikata facility has been put through a number of leachate tests including the Japanese JLT-46, NEN-7341 and the American TCLP analysis. These tests were conducted by two independent laboratories Shimadzu Techno-Research Inc. and ALS Laboratory Group. The results show that the Mihama-Mikata slag components are below the test detection limits and the slag is considered non- leaching. Below is a chart showing some of the results from the JLT-46 tests

| Heavy Metal | Unit | Method Detection Limit | Average Measured Value of Slag | JLT-46 Limit |
|-------------|------|---------------------------|-----------------------------------|--------------|
| Arsenic | mg/L | 0.001 | <0.001 | 0.01 |
| Cadmium | mg/L | 0.001 | <0.001 | 0.01 |
| Chromium VI | mg/L | 0.005 | <0.005 | 0.05 |
| Lead | mg/L | 0.001 | <0.001 | 0.01 |
| Mercury | mg/L | 0.0001 | <0.0001 | 0.005 |
| Selenium | mg/L | 0.001 | <0.001 | 0.01 |



PLASMA GASIFICATION TECHNOLOGY









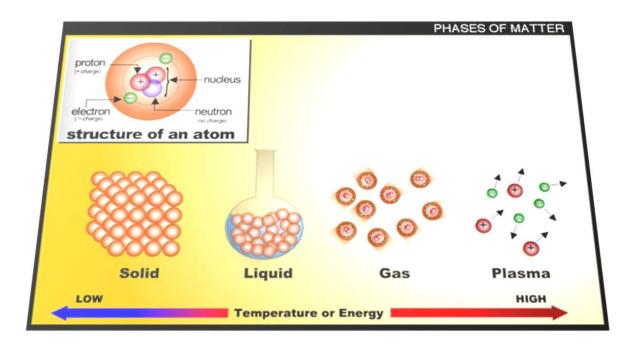
Origin of Plasma

- Plasma is a fourth state of matter
- Discovered by British physicist Sir William Crookes in 1879
- Heating a gas at very high temperature lead to ionization of atoms and turn it into plasma.
- Natural plasma can be seen in lightning, sun star, comet, etc..
- Firstly used by metal industry in 1800 in metallurgical, and in 1900 chemical industry to made acetylene from natural gas
- Plasma technology was used by NASA in 1960 and from this time become popular



WITAT IST LASPIA :

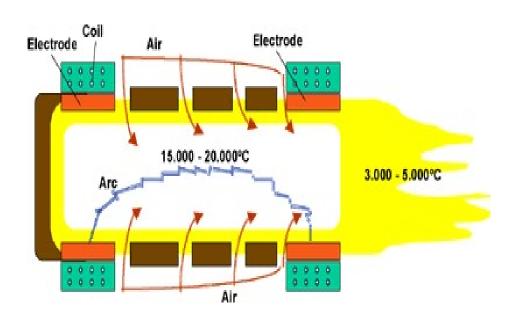
Plasma Gasification process is a drastic **non-incineration thermal process**, which uses extremely high temperatures in an oxygen-starved environment to completely decompose input waste material into very simple molecules.

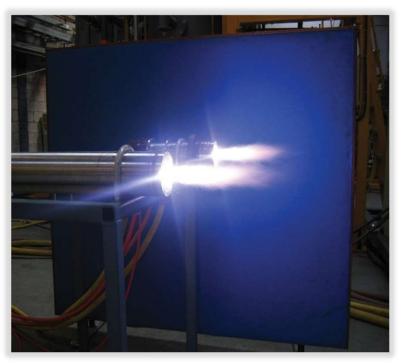




AIR PLASMA TORCH

The Plasma Torch is at the heart of our plasma waste processing and waste-to-energy technologies





Plasma is an ionized, conductive gas at a temperature till 5 000 °C, which arises when a stream of the carrier gas (air enriched with 93 % oxygen) is passed through an arc discharge.





PLASMA GASIFICATION vs INCINERATION

1.Absence of oxygen
2.Results in gas which can be used
to produce energy
3.Residue is an inert glass-like
slag
4.Residue amounts from around
6% to 15% of original solids
volume
5.Extremely low levels of

emissions

 Includes oxygen
 The energy will be converted in heat

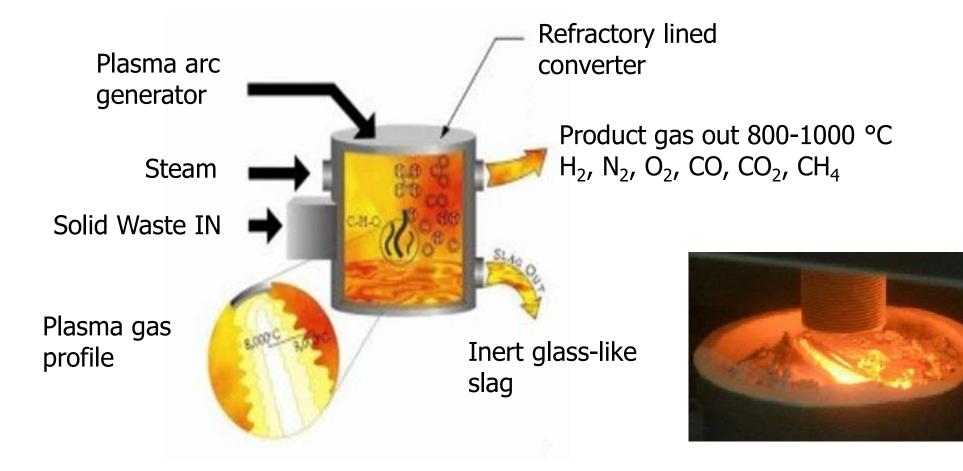
3.Residue is ash which is
considered a hazardous waste
4.Residue can be as much as 30%
of original solids volume
5.High level of emissions of GHG
and other pollutants

Incineration

Plasma Gasification

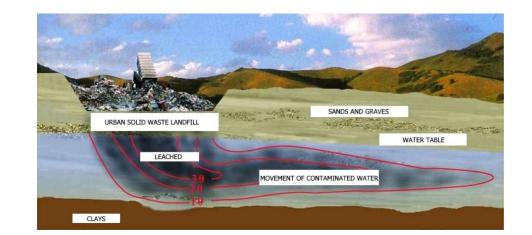


VITRIFICATION OF MSW (Municipal Solid Waste)





One of the great problems generated by landfills is the liquids that flow through the deposited waste and that ooze from them or are contained in, we call them leachates. Leachate is a liquid that percolates through deposited solid waste and extracts dissolved or suspended solid materials from them. The leachate is formed by the mixture of rainwater infiltrated into the reservoir and other products and compounds from the waste degradation processes.

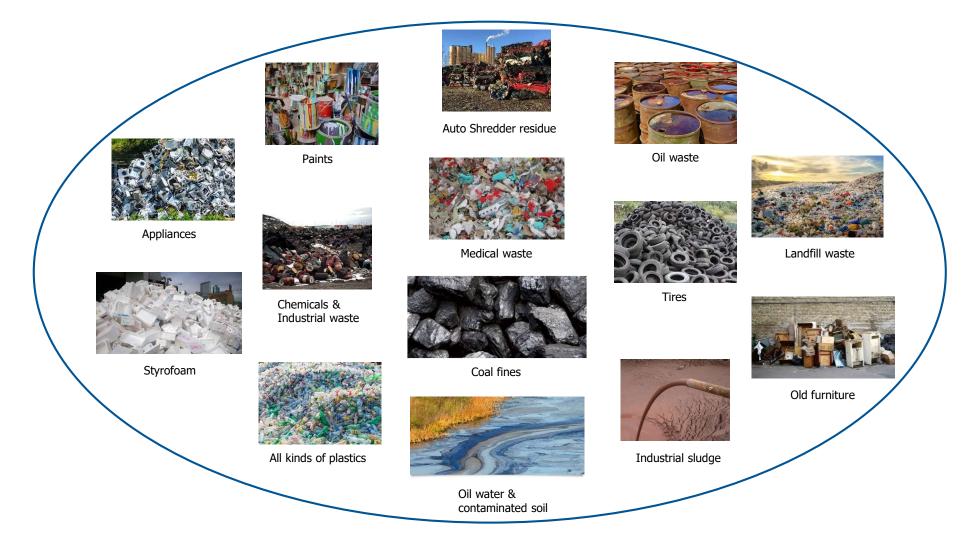


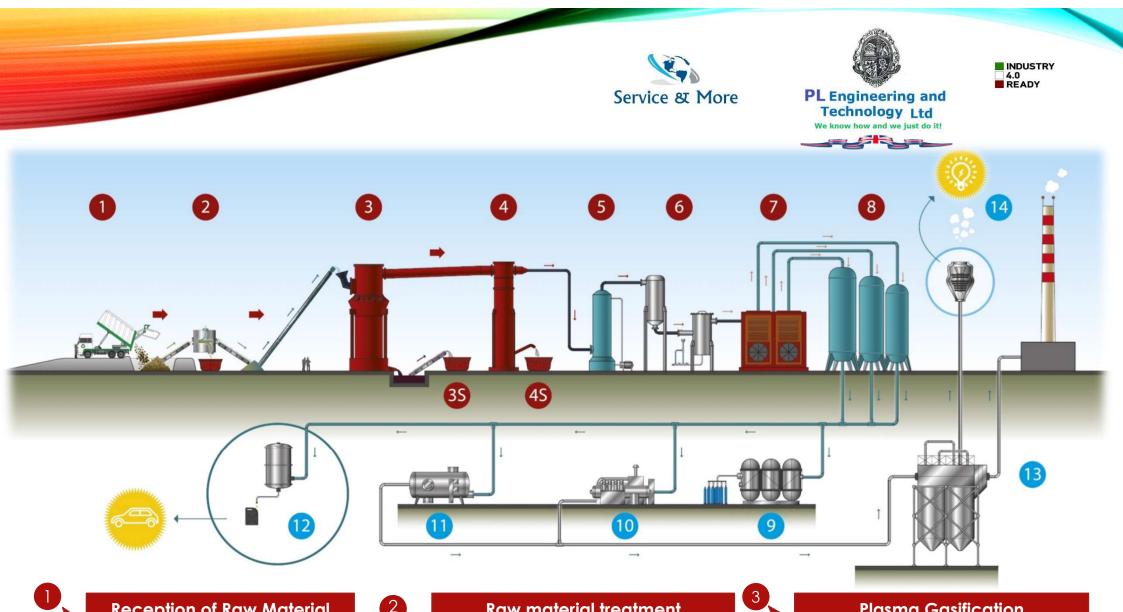
The leachates produced in our daily warehouse will be collected and sent to the plasma reactor through a pump.



WASTES HANDLED BY

This process is responsible for working all types of waste, including hazardous





Reception of Raw Material

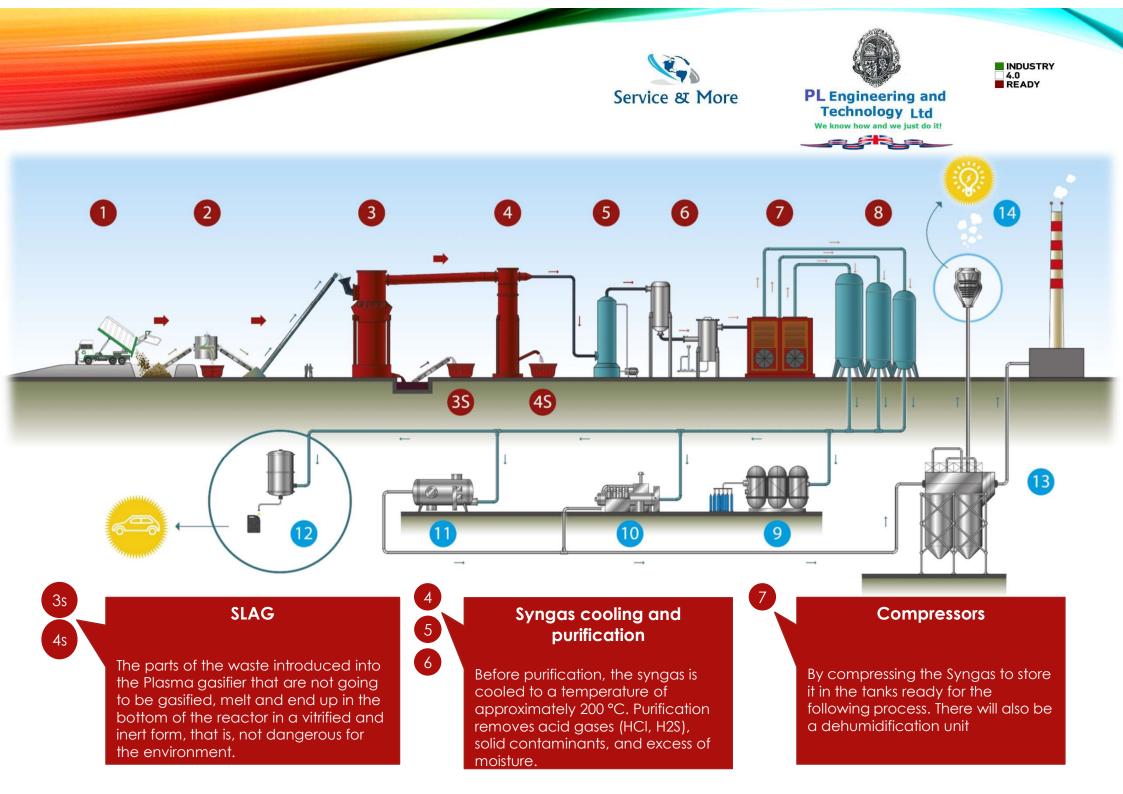
The garbage trucks will fill the tank which will have the size of at least the daily consumption of the plant, this to constantly feed the plant. The deposit will have a recovery of leachates that will be processed inside the reactor

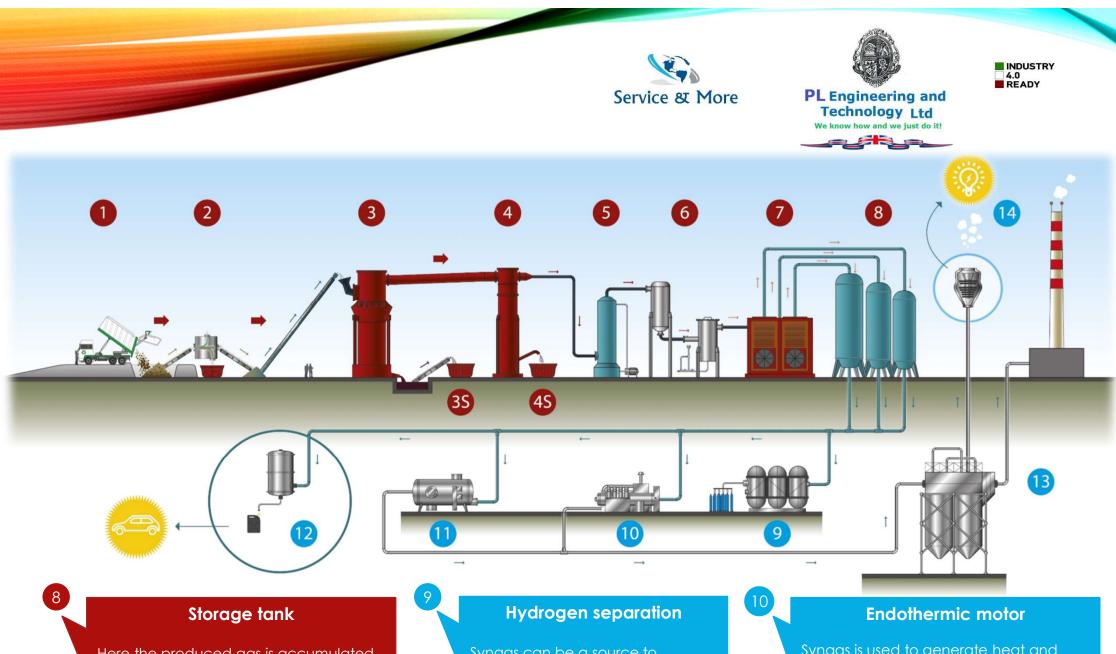
Raw material treatment

To convert waste into energy, first, it is necessary to select the raw material by removing as much material as possible that does not contain energy (for example, rubble, metals and glass). After this classification, the raw material is crushed, and then it is going to dry to get as much water as possible.

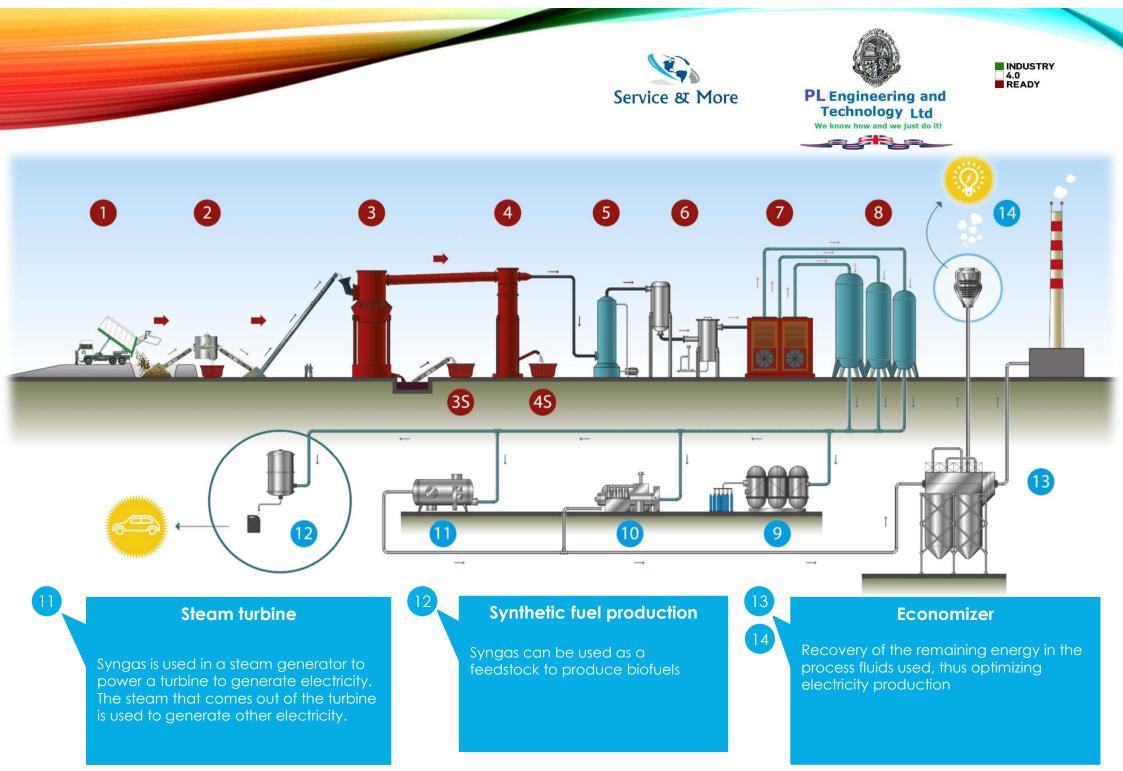
Plasma Gasification

Inside the reactor, the raw material is subjected to temperatures of 1250-1500 °C and comes into direct contact with the plasma discharge that has a temperature of 3000-5000 °C. Synthesis gas and slag are thus formed





Here the produced gas is accumulated before end use. They also serve to absorb irregular gas production and keep the supply constant for later uses. The amount of gas produced will be proportional to the type of waste that enters Syngas can be a source to produce hydrogen for various uses, including as an alternative fuel, in the hydrogenation industry, in the production of ammonia, etc. Syngas is used to generate heat and electricity in a cogeneration unit. Electricity production takes place through an internal combustion engine and an alternator that uses gas directly as fuel.







TRIAL WITH HAZARDOUS WASTE

| | Composit | ion | Parameters | Results |
|-----|--|---------------------------------|-----------------|-----------------------|
| | | | Feed rate | 1 TPD (42 kg/hr) |
| | | Waste residue | Mode | Continuous |
| 49% | 23% | Waste paint | Input power/hr | 10 KW |
| | 201/ | | Output power/hr | 52 KW |
| | 28% Chemical sludge | Net power output/hr | 42 KW | |
| | | Sluge | Syngas produced | 51 m ³ /hr |
| | | | Slag produced | 100 kg |

Power output = 1 MW/ton





TRIAL WITH BIOMEDICAL WASTE



| Parameters | Results |
|---------------------|-----------------------|
| Feed rate | 1 TPD (42 kg/hr) |
| Mode | Continuous |
| Input power/hr | 20 KW |
| Output power/hr | 80 KW |
| Net power output/hr | 68 KW |
| Syngas produced | 87 m ³ /hr |
| Slag produced | 80 kg |

Power output = 1.6 MW/ton





Container system to process Hospital waste Model : CTE 5 to 12

Hospital waste will be placed directly in a hopper without removing it from its protective bag or carton, and will be automatically ground, into the reactor. Thanks to the temperature in the reactor (from 3500 to 6000 degrees centigrade), the waste is automatically sterilized.

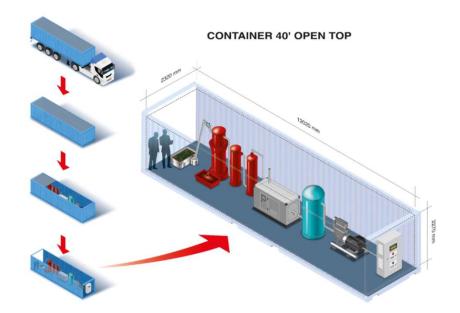
The Syngas produced will be filtered and sent to an endothermic engine with alternator to produce electricity.

The slag THE REACTION RESIDUE, about 4-8% of the waste introduced) are inert and reusable in the construction of buildings and roads. No operator comes into contact with infected waste during processing.

NB. In larger machines some components are placed in other containers (total n. 2 Containers)

TRIAL WITH BIOMEDICAL WASTE

| Parameters | Results | |
|---------------------|---------------------|--------------------|
| | MIN | MAX |
| Feed rate MIN | 2,5 TPD (100 kg/hr) | 12 TPD (500 kg/hr) |
| Mode | Continuous | Continuous |
| Input power/hr | 50 KW | 240 KW |
| Output power/hr | 200 KW | 960 KW |
| Net power output/hr | 150 KW | 720 KW |
| Syngas produced | 200 m3/h | 960 m3/h |
| Slag produced | Max 8% | Max 8% |



WARNING: PERFORMANCE ARE INDICATIVE AND DEPEND ON THE REAL COMPOSITION OF THE WASTE





TRIAL WITH OIL SLUDGE



| Parameters | Results |
|---------------------|------------------------|
| Feed rate | 1 TPD (42 kg/hr) |
| Mode | Continuous |
| Input power/hr | 32 KW |
| Output power/hr | 125 KW |
| Net power output/hr | 93 KW |
| Syngas produced | 126 m ³ /hr |
| Slag produced | 63 kg |

Power output = 2.2 MW/ton





TRIAL WITH TIRES



| Parameters | Results |
|---------------------|-----------------------|
| Feed rate | 1 TPD (42 kg/hr) |
| Mode | Continuous |
| Input power/hr | 20 KW |
| Output power/hr | 98 KW |
| Net power output/hr | 78 KW |
| Syngas produced | 97 m ³ /hr |
| Slag produced | 120 kg |

Power output = 1.8 MW/ton





TRIAL WITH PLASTICS



| Parameters | Results |
|---------------------|------------------------|
| Feed rate | 1 TPD (42 kg/hr) |
| Mode | Continuous |
| Input power/hr | 30 KW |
| Output power/hr | 120 KW |
| Net power output/hr | 90 KW |
| Syngas produced | 118 m ³ /hr |
| Slag produced | 60 kg |

Power output = 2.1 MW/ton





TRIAL WITH MSW (20% MOISTURE)



| Parameters | Results |
|---------------------|-----------------------|
| Feed rate | 1 TPD (42 kg/hr) |
| Mode | Continuous |
| Input power/hr | 35 KW |
| Output power/hr | 66 KW |
| Net power output/hr | 31 KW |
| Syngas produced | 65 m ³ /hr |
| Slag produced | 130 kg |

Power output= 0.6/0.7 MW/ton





ANALYSIS OF FLY ASH

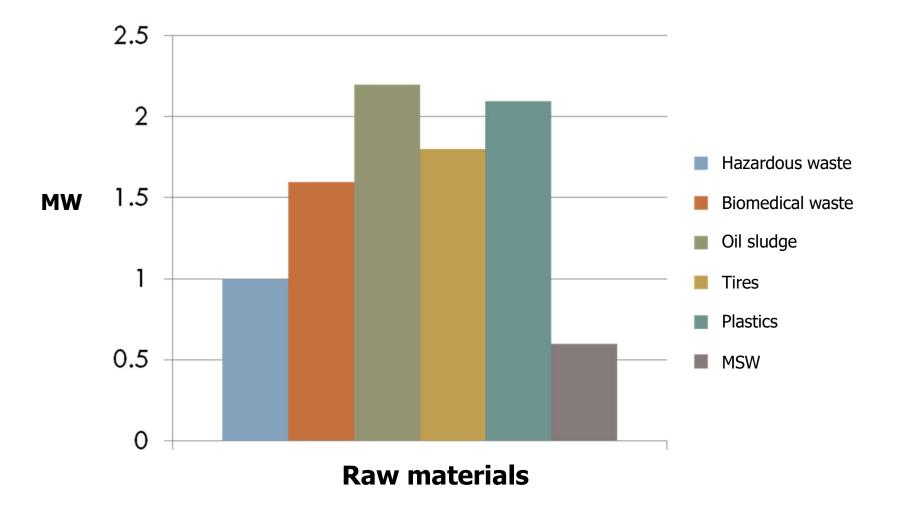


Plasma power=1000 Kwh/ton Volume reduction : 11:1

| Parameters | TCLP R | esults | |
|----------------------------|------------------|--------|-------|
| Feed rate | 1 TPD (42 kg/hr) | |) |
| Mode | Continuous | | |
| Heavy metals in ppm | Fly ash | Slag | Limit |
| Cd | 143 | 0.021 | 0.3 |
| Cu | 3640 | 0.332 | 3 |
| Zn | 2869 | 0.431 | - |
| As | 0.334 | 0.032 | 1.5 |
| Se | 1.33 | 0.022 | - |
| Pb | 11.19 | 1.198 | 3.0 |
| Cr | 1.17 | 0.004 | 1.5 |
| Density, kg/m ³ | 320 | 2770 | |
| Feed/slag output in kg | 1000 | 600 | |



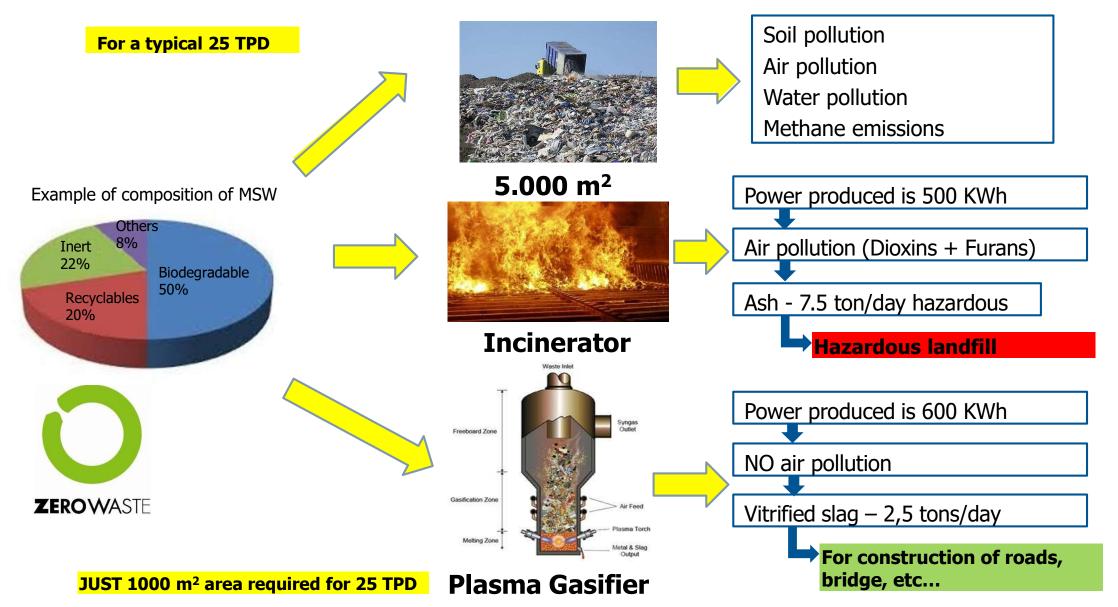
YIELD FOR DIFFERENT FEED TYPES







ZERO WASTE SCENARIO

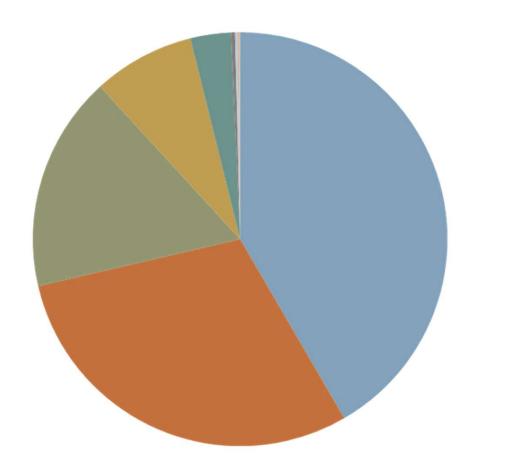




TYPICAL SINGAS COMPOSITION

Composition

| Hydrogen | <mark>44%</mark> |
|-----------------|--------------------|
| <mark>co</mark> | <mark>42%</mark> |
| Nitrogen | <mark>2%</mark> |
| CO ₂ | <mark>8%</mark> |
| CH₄ | <mark>3.20%</mark> |
| O ₂ | 0.30% |
| Acetylene | 0.20% |
| Ethylene | 0.10% |
| Otros | 0.10% |



HydrogenCO

- Nitrogen
- CO₂
- CH₄
- O₂
- Acetylene
- Ethylene
- Otros



EMISSIONS

| Parameters | Units | US EPA standards | EPA standards | Plasma emissions |
|-----------------|---------|---------------------|------------------|---------------------|
| Nox | ppmvd | 150 | 250 | 35-40 |
| PM | mg/dscm | 20-24 | 34 | <5 |
| SO ₂ | ppmvd | 30 | 55 | <2 |
| HCI | ppmvd | 25 | 15 | <10 |
| CO | ppmvd | 100 | 40 | <20 |
| Hg | µg/dscm | 50-80 | 55 | <2 |
| PCDD/ PCDF | ng/dscm | 13-30 | 25 | 0 |

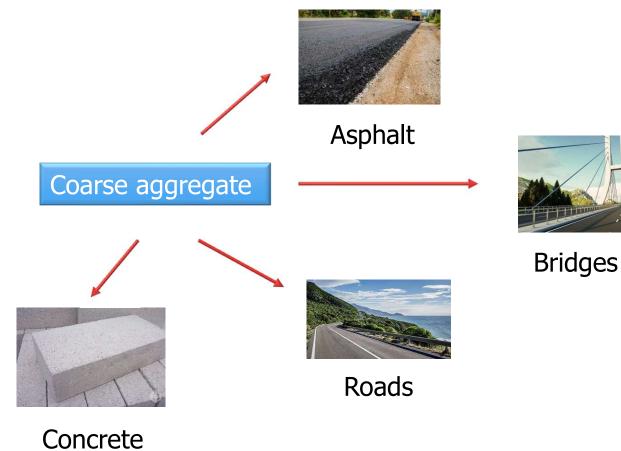




FROM MUNICIPAL SOLID WASTE, COAL ASH AND SLAG FOR SECONDARY USE:

Possible use of residual products:









Insulation





VITRIFIED SLAG TCLP

| Metal | Allowed concentration (mg/l) | Concentration (mg/l) |
|----------|------------------------------|----------------------|
| Arsenic | 5.0 | < 0.1 |
| Barium | 100.0 | < 0.5 |
| Cadmium | 1.0 | < 0.02 |
| Chromium | 5.0 | < 0.2 |
| Lead | 5.0 | < 0.2 |
| Mercury | 0.2 | < 0.01 |
| Selenium | 1.0 | < 0.1 |
| Silver | 5.0 | < 0.5 |
| | | |



WHAT ARE THE ADVANTAGES ?

- Gasification technology that works at atmospheric pressure, elevated temperature for a better transformation into gas
- > Feeding capacity with **any types of waste**, **solid**, **liquid**, **gas** (non-radioactive) and bio fuels
- Compact and modular, a feature that allows it, unlike traditional incinerators, to work from 30% to 100% of their nominal power, thus guaranteeing the operator the possibility of easily eliminating seasonal variations in the waste flow.
- Non-polluting and environmentally safe
- > High recovery of clean renewable energy such as electricity
- Excellent ROI (Return on Investment) ratio
- Consolidated technology
- Ready for circular economy
- Low start-up and shutdown time
- > Low GHG emissions





| Plasma-steam gasification | Plasma | Pyrolysis | Incineration |
|---------------------------------|--------------------------------|-------------------------------|---------------------------------|
| Total decomposition (2000°C) | ✓ (3000-5000°C) | Decomposition at 90% (800°C) | Decomposition at 70% (1000°C) |
| Combustion type | Indirecta | Indirect | Direct |
| Absence of resins and | \checkmark | Presence of resins and furans | Massive presence of resins and |
| furans | | | furans |
| Ash absence | \checkmark | 10% ash | 30% toxic ash |
| Any type of waste | \checkmark | Х | Х |
| No need to sort waste | \checkmark | Х | Х |
| Exhaust gas emissions | Low | Medium | Elevated |
| Unaffected by the moisture | \checkmark | Х | Х |
| content of the waste. | | | |
| Sublimation | \checkmark | Х | Х |
| Modularity | \checkmark | Х | Х |
| Construction time | 12-15 meses | 12-15 meses | 5 años |
| Waste | Obsidian | - | Ashes |
| Plant size | Small | Medium | Big |
| Plant waste products | 100% recyclable inert material | - | Dangerous ash to be disposed of |
| | | | in landfills |
| Emissions | | | |
| NOx | <36 ppmvd | | <110-205 ppmvd |
| SO ₂ | <1.05 ppmvd | | <26-29 ppmvd |
| Нд | <1.4 µg/dscm | | <28-80 µg/dscm |





FACILITIES







FACILITIES













FACILITIES

INDUSTRY 4.0 READY







QUALIFICATIONS



International Union of Professional Engineers



The Society of Professional Engineers Ltd - UK CERTIFICATE OF QUALIFICATION PROFESSIONAL ENGINEER



CERTIFICATE OF QUALIFICATION PROFESSIONAL ENGINEER - GERMANY



"Finding it's a beginning, staying together is a progress, working together is a success"

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